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(54) Olefinic polymerisation using silyl ether initiators

(57) Process for anionically polymerising a conjugated 1,3-diene monomer consists of contacting the monomer in an inert hydrocarbon solvent with a monofunctional silyl ether initiator of general formula



where R¹ to R³ are independently selected from monovalent organic substituent groups and A is a short chain hydrocarbon bridging group, to yield a polydiene having a molecular weight of typically 1,000–10,000, a high 1,4 content of typically 90% and a low polydispersity of typically 1.15. The reactive ends of the living polymer chains may be terminated with a reactive group such as hydroxyl by treating the polymer with ethylene oxide. Subsequent removal of the polymer's relatively unreactive silyl end groups by reaction with tetra-n-butylammonium fluoride produces a difunctional, chain-extendable, hydroxy-terminated polydiene useful as a rubbery binder prepolymer.

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PROCESS FOR THE POLYMERISATION OF OLEFINIC - CONTAINING MONOMERS
EMPLOYING ANIONIC INITIATORS

5 This invention relates to a process for the polymerisation of
olefinic-containing monomers employing anionic initiators. The
invention also relates to novel anionic initiators for use in said
process, and to polymers produced by said process.

10 Highly useful polymeric products can be obtained by
polymerising olefinic-containing monomers in the presence of an
organo-alkali metal initiator and subsequently reacting the
resulting polymer, containing an active alkali metal end group or
groups, with a reagent which will either couple the polymer
molecules or replace the alkali metal with more stable reactive end
15 groups.

It can be seen that such a polymerisation process will consist
essentially of three stages:

- 20 a. Initiation, in which the monomeric material is contacted
with a monofunctional or difunctional anionic initiator.
- b. Propagation, in which the monomer is allowed to
polymerise to form living polymer chains with negatively
25 charged ends, and
- c. Termination, in which the living polymer chains are
treated with suitable reagents, generally to form
monofunctionally or difunctionally terminated polymers.

30

The presence of a reactive terminal group or groups on the ends
of the polymer molecules enables substantially more effective cures
to take place. In the case of a polymer containing a reactive group
on each of its ends (a telechelic polymer) all of the polymer
35 molecule will be tied into the cross-linked structure of the cured
material.

The well defined structure produced by telechelic polymers in the networks of their cured products is the primary reason for their increased use as precursors in the commercial production of cured rubbery solids.

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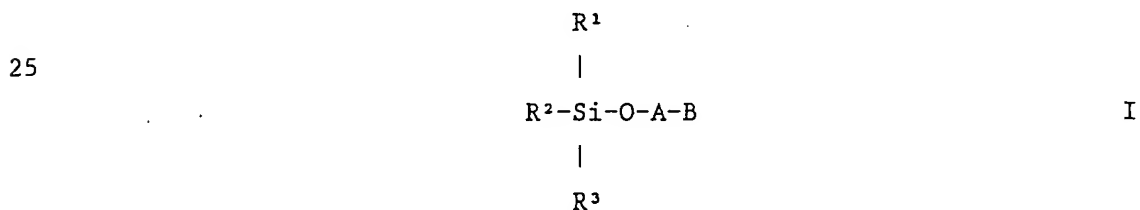
However, in order to meet the requirements of a modern synthetic rubber it is not enough that the polydiene produces effective cures nor that the cured product has a well defined cross linked structure, it is also important that the cured product possesses good elastomeric properties. In the case of polydienes the elastomeric quality of the cured product is dependent upon the 1,4-content of the polymeric diene. Generally, the higher the 1,4-content of the polymer, the lower its glass transition temperature and the better the elastomeric properties of the cured product. It follows from this that any process chosen for the commercial production of polydienes (in particular telechelic polymers of 1,3-dienes) must lead to a material having a high 1,4-content.

20 It is well known that monofunctional polyalkenes and high 1,4-content monofunctional polydienes can be prepared in inert non-polar hydrocarbon solvents by initiating the reaction with a monofunctional anionic initiator such as butyl lithium. The preparations of telechelic polydienes, using corresponding
25 difunctional initiators such as 1,4-dilithiobutane, has hitherto required that the anionic polymerisation reaction (propagation) takes place in the presence of a sterically-hindered Lewis acid in order to ensure that the polymeric product possesses a reasonable 1,4-content (typically 25-50%). Furthermore, the polymerisation
30 reaction must take place in polar solvents such as alkyl and cycloalkyl ethers because difunctional initiators are insoluble in non-polar solvents such as hydrocarbons, and this has hitherto prevented the formation of polydienes with 1,4 contents above about 50% which can be produced using the aforementioned monofunctional
35 initiators in hydrocarbon solvents.

A further disadvantage associated with the use of difunctional initiators is that the choice of telechelic polymers which can be produced at the termination of propagation is restricted to those having identical terminal groups at either end since the reagent
 5 used for termination will react in a similar manner with both living ends of the growing polymer chain.

The main object of the present invention is to provide a new process for the anionic polymerisation of an olefinic-containing
 10 monomer which can be used to prepare telechelic polymers and yet avoids the disadvantages associated with the use of known difunctional initiators. It is a further object of the present invention to provide a process for the anionic polymerisation of a conjugated 1,3-diene which produces a polymeric material having an
 15 enhanced 1,4-content. It is a yet further object of the invention to provide a novel anionic initiator for use in the present process.

According to the present invention, there is provided a process
 20 for the anionic polymerisation of an olefinic-containing monomer comprising contacting the monomer in an inert solvent with a monofunctional silyl ether initiator of general formula I



30 wherein R^1 , R^2 and R^3 are independently selected from saturated and unsaturated aliphatic and aromatic radicals, A is a hydrocarbon bridging group containing from 1 to 25 carbon atoms and B is an alkali metal.

The inert solvent is preferably a non-polar solvent such as a hydrocarbon, since anionic polymerisation in the presence of such solvents is known to produce, from 1,3-dienes, polydienes with high 1,4-contents. Preferred solvents are aliphatic, alicyclic and aromatic hydrocarbons, especially alkanes, cycloalkanes and cycloalkenes, having from 3 to 12, preferably from 4 to 8, carbon atoms. Examples of suitable hydrocarbons are hexane, cyclohexane, toluene and benzene. Alkanes are the most preferred solvents.

The olefinic monomer is preferably an alkene or a 1,3-diene. The alkene or 1,3-diene will be chosen from the group of unsaturated organic compounds that can be polymerised anionically (ie in a reaction initiated by an organo alkali metal). Suitable alkenes include the optionally-substituted styrenes and vinylnaphthalenes. Suitable 1,3-dienes will preferably contain from 4 to 12, especially from 4 to 8, carbon atoms per molecule. Examples of these compounds include the following: 1,3-butadiene; isoprene; 2,3-dimethyl-1,3-butadiene; 1,3-pentadiene; 2-methyl-3-ethyl-1,3-butadiene; 3-methyl-1,3-butadiene; 2-methyl-3-ethyl-1,3-pentadiene; 1,3-hexadiene; 2-methyl-1,3-hexadiene; 1,3-heptadiene; 3-methyl-1,3-heptadiene; 1,3-octadiene; 3-butyl-1,3-octadiene; 3,4-dimethyl-1,3-hexadiene; 3-n-propyl-1,3-pentadiene; 4,5-diethyl-1,3-octadiene; phenyl-1,3-butadiene; 2,4-diethyl-1,3-butadiene; 2,3-di-n-propyl-1,3-butadiene; and 2-methyl-3-isopropyl-1,3-butadiene.

Among the dialkylbutadienes, it is preferred that the alkyl groups contain from 1 to 3 carbon atoms. Of the above monomers 1,3-butadiene, isoprene, 2,3-dimethyl-1,3-butadiene and 1,3-pentadiene are preferred with 1,3-butadiene being particularly preferred. The dienes may be polymerised alone, or in admixture with each other or with alkenes to form random copolymers, or by charging the dienes to the reaction mixture sequentially, either with each other or with alkenes, to form block copolymers.

R^1, R^2 and R^3 are preferably independently selected from alkyl, alkoxy, aryl, and alkaryl. More preferably, each of the radicals R^1, R^2 and R^3 contains from 1 to 10 carbon atoms. In order to reduce the reactivity of the siloxy group on the initiator, the radicals R^1, R^2 and R^3 are preferably not all methyl and preferably together contain at least 4, most preferably at least 5, carbons atoms. In this way, a degree of steric hindrance is introduced into the silyl group which inhibits reaction between that group and the living ends of the growing polymer chain, especially when at least one of R^1, R^2 and R^3 contain at least three, more especially at least four, carbon atoms. Polymer yield and purity is also generally enhanced if at least one of R^1, R^2 and R^3 is aryl, preferably phenyl or mono-substituted phenyl with the mono-substituent group on the phenyl preferably being a C_1-C_5 alkyl group.

The spacer group A is preferably contains at least two carbon atoms and is preferably a saturated hydrocarbon group such as a branched or straight chain alkyl bridging group, though less preferably it may contain at least one aromatic group such as a p-phenylene group. The principal criteria for the selection of the group A is that it should be sufficiently long to prevent the siloxy end group from interfering with the polymerisation reaction, and it should provide the initiator with enhanced solubility in the inert, preferably non-polar solvent employed in the process. At the same time it should not add significantly to the size and bulk of the terminal group at the end of the polymer chain because this will adversely affect the polymer's physical properties, especially its elastomeric properties. For these reasons, A is most preferably a straight chain alkyl bridging group of formula $-(CH_2)_m-$ where m is an integer from 3 to 15, especially 3 to 10.

B is preferably lithium or sodium, and is most preferably lithium.

The present polymerisation reaction is preferably carried out at a temperature of between -30°C and $+30^{\circ}\text{C}$, especially between -10°C and $+10^{\circ}\text{C}$. The maximum temperature that may be employed in a given system will depend primarily on the physical properties, especially the boiling points, of the monomers and solvent chosen.

The amount of initiator added to the reaction mixture will be determined by the structure of the monomer to be polymerised and by the desired molecular weight of the polymer. Typically for the production of a polymer containing a polymeric chain, derived from the polymerisation of an olefinic-containing monomer and having a polymer molecular weight between about 1,000 and 100,000, between 0.5 and 50 mmoles of initiator is used for each mole of monomer. The polymeric chain preferably has a molecular weight in the range 1,000 to 10,000 in which case preferably between 5 and 50 mmoles of initiator is used for each mole of monomer.

After propagation has been allowed to reach equilibrium, the single active ends on the living polymer chains may be terminated, by the addition of suitable reagents which either donate a proton to or functionalise the anionic carbons. Proton donors such as water or alcohol yield terminally non-functional polymers. Preferably, however, the polymer chains will be terminated by a functional group. Examples of suitable end groups are:

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a. hydroxyl, prepared by adding aldehydes, ketones or alkylene oxides, especially ethylene oxide;

30

b. carboxyl, prepared by adding CO_2 to the anionic polymer;

c. mercapto, prepared by adding sulphur, cyclic disulphides or cyclic sulphides such as ethylene or propylene sulphides;

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d. amino and aziridine, prepared by adding aminoaldehydes or polyaziridines such as phenyl-bis(2-methyl-1-aziridinyl) phosphine oxide;

e. epoxide, prepared by adding glycidaldehyde or diepoxides;
and

5 f. metal halides, especially magnesium halides, prepared by
adding a metal halide such as magnesium bromide.

Alternatively, the living polymer chains may be terminated by a
di-or polyfunctional coupling agent which is capable of terminating
two or more polymer chains through a single coupling agent molecule,
10 thereby linking those chains together, with the advantage that a
considerable increase in polymer molecular weight can be achieved
with little degradation in polydispersivity. An example of such a
coupling agent is SiCl_4 , which by displacement of its chloro
substituent groups yields a "star" polymer with four, organosiloxy-
15 terminated polymer chains radiating from a central silicon atom.
Other polymers containing from 2 to 20 polymer chain arms radiating
from a central coupling agent may be prepared utilising complex
coupling agents such as multi-functional organohalides typically
containing from 2 or 3 to 20, preferably 2 to 4, halide groups, and
20 other multi-functional polyhalosilanes preferably containing from 2
to 4 halide groups. Examples of such coupling agents are 1,2
ethylene dibromide, 1,4 dichlorobutane, and dimethyldichlorosilane.

The organosiloxy protective groups remain unaffected by these
25 various termination reactions. However, once propagation has been
terminated, the relatively inert organosiloxy end groups on the
polymer chains may then be functionalised by reaction with a
desilylation reagent to yield, after subsequent reaction with acid
solution, reactive hydroxyl end groups which are reactive in the
30 sense that they can be reacted further to give rise to chemical
cross-linking of the polymer chains. Preferred reagents for such
desilylation reactions are the tetralkylammonium fluorides,
especially tetra-n-butylammonium fluoride, in polar solvents such as
alkyl or cycloalkyl ethers, especially tetrahydrofuran. These and
35 other suitable desilylation reagents are discussed in Synthesis, 9,

817-845 (1985), especially on page 828. Since aziridine and epoxide groups may react with some of these reagents and/or acid solutions, these groups represent less preferred terminal groups on the other ends of the polymer chains prior to desilylation.

5

The present polymerisation process offers a number of significant advantages over other known anionic polymerisation processes. First, the molecular weight distribution (M_w/M_n) is narrower than that achieved by the analogous reaction using difunctional anionic initiators. In the present case the molecular weight distribution (also known as "polydispersivity") is typically about 1.1 whilst in the competing process M_w/M_n is for a polydiene generally 1.5 or above in the absence of sterically-hindered Lewis acid and about 1.3 in the presence of a sterically-hindered Lewis acid. The advantage offered by a polymer with a narrow M_w/M_n is that it produces a cured product with a well defined network and, as a consequence, high strength.

The second advantage offered by the present process is the enhancement of the 1,4-content of the polydiene products it is capable of producing from the anionic polymerisation of 1,3-dienes. In the present process, polydienes with a 1,4-content of 90% can be routinely prepared, whereas with difunctional initiators, the maximum 1,4-contents achievable is about 50%. This advantage stems principally from the advantageous solubility of the present initiator compounds in inert, non-polar hydrocarbon solvents which obviates the need to conduct polymerisation within a polar solvent.

A third advantage of the present invention is that it allows for the preparation of polymers with a far greater diversity of functionality than has hitherto been achievable by anionic polymerisation. Monofunctional polymers result from termination with a proton donor followed by reactive functionalisation of the

organosiloxy end groups (for example, to produce reactive hydroxyl end groups). Bifunctional (telechelic) polymers result from (a) functional termination of the polymerisation reaction followed by (b) reactive functionalisation of the organosiloxy end groups.

- 5 Indeed this can lead to telechelic polymers having the same or different functional end groups depending on the reagents used in each of the steps (a) and (b), adding further to the aforesaid advantage of diversity. Di- and poly-functional polymers result
- 10 from termination of the polymerisation reaction with di- and poly-functional coupling agents, followed by reactive functionalisation of the organosiloxy end groups.

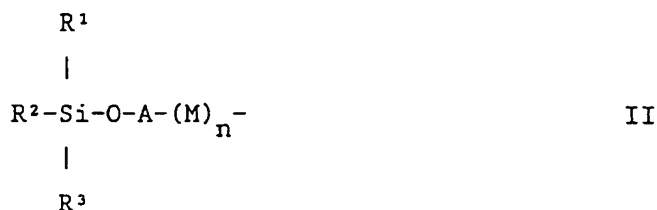
The terminated polymers resulting from the present process

15 represent a novel group of polymers which may be used as intermediates in the preparation of further, functionally terminated polymers, especially telechelic polymers, by the subsequent conversion of the protective organosiloxy end groups into hydroxyl functional groups.

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According to a further aspect of the present invention, therefore, there is provided a siloxy-terminated hydrocarbon polymer containing at least one polymer chain per molecule of general formula II

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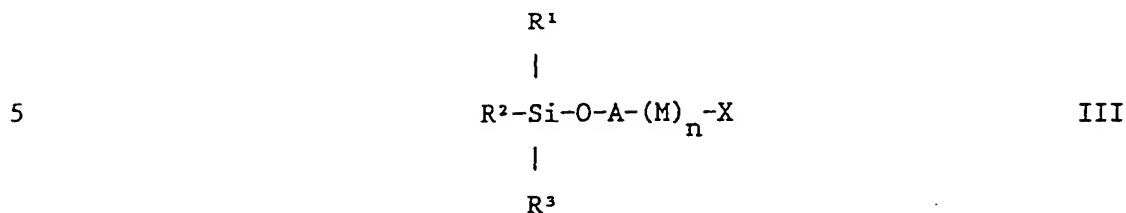


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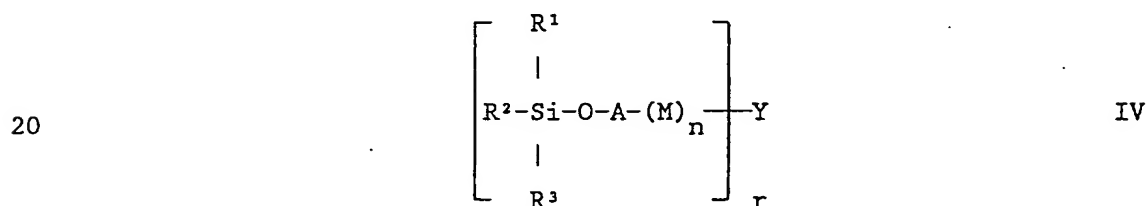
wherein R^1, R^2, R^3 and A are as defined above, and $-(M)_n-$ represents

35 a polymerised olefinic-containing monomer, preferably a polymerised alkene or, more preferably, a polymerised 1,3-diene.

The polymer may be of general formula III



10 wherein X is selected from H, carboxyl, hydroxyl, mercapto, amino and a metal halide, especially a magnesium halide, group. Such polymers are produced by terminating the living polymer chain produced by the present process by the monofunctional reagents described above. Alternatively, the polymer may be of general
15 formula IV

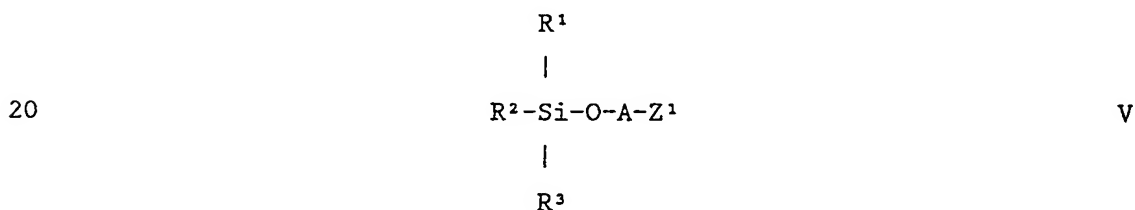


wherein Y is the residue of a di- or multi-functional halide
25 coupling agent containing q functional halide groups, where q is an integer from 2 to 20 (for example, 3), especially from 2 to 4, and r is an integer of at least 2 (for example, 3) which is less or equal to q. For example, four-chain polymers of general formula IV linked together by a single silicon atom can be produced by living chain
30 termination with the polyfunctional coupling agent $SiCl_4$. Similarly, polyfunctional organohalide coupling agents such as 1, 2 ethylene dibromide and 1,4 dichlorobutane, and other polyfunctional polyhalosilane coupling agents such as dimethyldichlorosilane, may also be used.

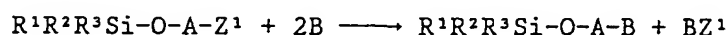
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Preferably, the polymeric chain $-(M)_n-$ has an average molecular weight in the range of 1,000 to 10,000, especially 2,000 to 7,000 in which case the polymers produced by the present invention will, if
 5 the polymer molecules contain a single polymeric chain $-(M)_n-$, normally be liquids. If desired however semi-solid and solid polymers with polymeric chains $-(M)_n-$ having an average molecular
 10 weight of up to 100,000 or above may also be prepared.

According to a further aspect of the present invention, there are also provided novel monofunctional silyl ether initiators which are suitable for use in the present process. These novel initiators
 15 may be prepared by the method of reacting, in an inert solvent, the alkali metal B with an organosiloxyhalide of formula V



wherein R^1, R^2, R^3 and A are as defined above and Z^1 represents a
 25 halogen. The reaction may be represented by the equation



Z^1 is preferably chlorine or bromine, and is most preferably
 30 chlorine.

The reaction, which is exothermic, is preferably performed in a non-polar solvent. Preferred solvents are aliphatic, alicyclic and aromatic hydrocarbons, especially alkanes, cycloalkanes and
 35 cycloalkenes, having from 3-12, preferably from 4-8, carbon atoms. Most preferably, the solvent is the same as that used in the subsequent polymerisation reaction.

The alkali metal B, which is preferably lithium, is preferably provided in particulate form such as chopped fine wire (typically 1-2mm diameter) or freshly cut chips. The particles are preferably subjected to high speed agitation in a fluid suspension prior to use to produce a clean metallic surface for further reaction. If lithium is used, then it preferably contains from 0.5-3%, more preferably 1-2%, by weight of sodium. In the absence of sodium, lithium tends to be unreactive towards organic halides. However, with increasing sodium content, there is an increasing likelihood of undesirable side reactions and above 5wt% sodium, the reagents may react violently. It has been found that in order to ensure a high yield of product initiator, a stoichiometric excess of alkali metal must be used, of preferably at least 1½-fold, more preferably at least two-fold, most preferably at least 2½-fold, with an upper limit of preferably six-fold.

The reaction is preferably performed at a temperature of from 10°C to 50°C, more preferably from 20°C to 40°C. At temperatures above about 40°C, the production of undesirable organic by-products is observed. The temperature can be controlled by cooling the reaction, and by ensuring that the major part of the organosiloxyhalide co-reagent is added slowly to the alkali metal already in situ within the solvent. A reaction temperature of at least 30°C is most preferred especially if the solvent is non-polar, to ensure that the reaction goes substantially to completion.

A further preferred condition of the reaction is that it should be performed under a dry, oxygen-free inert gas. The gas is preferably a noble gas such as helium or argon, since nitrogen will react with the alkali metal to form a metal nitride, especially if the metal is lithium.

The advantage of this method of initiator preparation is that the principal by-products of the reaction (alkali metal halide and excess alkali metal) are insoluble inorganic solids rather than

reactive, solvent-soluble organic compounds and so are easily separated from the soluble initiator compound before it is used in the subsequent polymerisation process.

- 5 The organosiloxyhalide compound of general formula V may be prepared by reacting, in an inert solvent an alcohol of general formula VI



10

with a silylhalide of general formula VII



15

wherein Z^2 is a halogen which is the same or different to Z^1 and is preferably chlorine.

20

The present invention will now be described by way of Example only.

25 Materials

Butadiene (Matheson) was dried by passage through molecular sieves, calcium chloride and calcium hydride, before collecting in a graduated vessel at -78°C .

30

Diethylether (BDH) was dried overnight over freshly cut sodium metal (2mm diameter wire), filtered and used immediately.

Diphenylacetic acid (BDH) was stored at 40°C under vacuum for at least 24 hours before use.

35

Hexane (BDH) was dried over calcium hydride and fractionally distilled under nitrogen, the fraction boiling at 67-8°C being collected. Lithium metal (Fluka) containing 1-2% sodium was supplied as a 30% w/w dispersion in mineral oil. The metal was washed repeatedly with hexane before charging with the reaction solvent so as to prepare a clean silvery white metal surface.

Tert-butyldimethylsiloxy 1-chloro-hexyl ether was fractionally distilled, under reduced pressure prior to use, the fraction boiling at 184-5°C (100mmHg) being collected.

Tert-butyldiphenylsiloxy 1-chloro-hexyl ether was distilled from a kugelrohr (oven temperature 215°C) under reduced pressure (1mmHg), just prior to use.

Tert-butyldiphenylsiloxy 1-chloro-propyl ether was distilled from a kugelrohr (oven temperature 200°C) under reduced pressure (1mmHg), just prior to use.

Tetra-n-butylammonium fluoride (Aldrich) was supplied as a 1.0M solution in tetrahydrofuran and used directly.

Tetrahydrofuran (BDH), stabilised with 0.1% quinol, was distilled under nitrogen when required after sufficient sodium benzophenone solution in THF had been added to yield a permanent purple colour.

General Procedure

All experimental techniques were performed under an inert atmosphere, be it oxygen-free nitrogen or argon. All glassware, except syringes, was cleaned by successive washing with 10% hydrofluoric acid, distilled water and acetone. It was then dried and stored in an oven at 120°C until required. All additions, excepting that of alkali metals, were performed via syringe.

Example 1

A sixfold excess of lithium slurry (10g) in mineral oil was placed into a 500ml 3-necked round bottom flask equipped with serum cap, argon inlet/outlet, water condenser, thermometer and magnetic follower. The slurry was then repeatedly washed with hexane, by high speed agitation, until a clean silvery white metal surface was obtained. The lithium metal was then charged with further hexane (100ml) which was to act as the reaction solvent. The temperature inside the reaction flask was then raised to 35°C and allowed to reach thermal equilibrium over the space of thirty minutes.

Freshly distilled tert-butyldimethyl (tBDM-) siloxy-1-chlorohexyl ether (5g, 0.02 mol) was injected into the reaction vessel. A primary exotherm was observed to commence after 5-10 minutes. This exotherm was controlled by the utilisation of cold air cooling which maintained the flask temperature below 45°C throughout the course of the reaction. Four further aliquots of tBDM-siloxy-1-chlorohexyl ether (4 x 5g, 0.08 mol) were added over a period of 1-2 hours. The reaction was allowed to proceed for a further 2 hours before allowing the products to settle inside the flask. The crude supernatant hexane solution of tBDM-siloxy-1-lithiohexyl ether could then be extracted via syringe and utilised in various reactions, or simply quenched with methanol to produce tBDM-siloxy hexane (Yield 95%). The yield of the reaction was confirmed by ¹H n.m.r. spectroscopy and i.r. spectroscopy.

Example 2

The procedure of Example 1 was repeated except that the species to be lithiated was tert-butyldiphenyl (t-BDP-) siloxy-1-chlorohexyl ether rather than tert-butyldimethylsiloxy-1-chlorohexyl ether. The resultant yield of the reaction was again greater than 90%.

Example 3

The procedure of Example 1 was repeated except that the reaction was executed within the temperature range 20-30°C, and the reaction solvent was diethylether instead of n-hexane. The resultant yield of the reaction was again greater than 90%.

Example 4

The procedure of Example 1 was repeated except that the species to be lithiated was tert-butyldiphenylsiloxyl-1-chloropropyl ether rather than tert-butyldimethylsiloxyl-1-chlorohexyl ether. The reaction was executed within the temperature range 20-30°C, and the reaction solvent was diethylether instead of n-hexane. The resultant yield of the reaction was again greater than 90%.

Example 5

The procedure of Example 1 was repeated except that the species to be lithiated was tert-butyldiphenylsiloxyl-1-chloropropyl ether rather than tert-butyldimethylsiloxyl-1-chlorohexyl ether. The reaction was executed within the temperature range 20-30°C. The resultant yield of the reaction was only 25% after 17 hours.

TABLE 1

The Effect of Temperature and Solvent Upon the Preparative Yield of Trialkyl/aryl Siloxy Lithioalkyl Ethers

Trialkyl/Arylsiloxyl Lithioalkyl Ether	Solvent	Temperature	Yield
tBDM-siloxyl lithiohexyl ether	Hexane	35-40°C	>90%
" " "	Ether	20-30°C	>90%
tBDP-siloxyl " "	Hexane	35-40°C	>90%
tBDP-siloxyl lithiopropyl ether	Ether	20-30°C	>90%
" " "	Hexane	20-30°C	25%

Example 6

Hexane (250ml) was placed in a 500ml round bottom 3-necked flask equipped with magnetic follower, thermometer, serum cap and nitrogen inlet/outlet. The reaction vessel was then chilled to -78°C and butadiene (30ml) distilled into the system. The reaction mixture was then gradually allowed to warm to -5°C and tBDM-siloxyl 1-lithiohexyl ether (0.011 mol) in hexane solution from Example 1 was introduced by injection in order to initiate polymerisation. Propagation was allowed to proceed at this temperature for an hour, before the ice bath was removed and the reaction mixture gradually allowed to reach room temperature. Propagation was then allowed to continue at room temperature for a further 16 hours. Termination of the living ends was then accomplished typically by the injection of a five-fold excess of methanol (1ml) to yield a water white polymer solution. This was subsequently reduced in volume by rotary evaporation, precipitated into excess methanol (1000ml) and the crude polymer syrup collect on decanting. The work up produced a monofunctional polybutadiene with a siloxyl group on one end of the polymer chain. The product was found to be of low molecular weight (2,100), to be relatively monodisperse ($M_n/M_w=1.1$) and to possess a high 1,4 percentage content (89%).

The molecular weight of the product was determined by gel permeation chromatography (gpc) in which measurements were carried out using a Waters 840 chromatograph fitted with refractive index and ultra-violet detectors in series. Four styragel columns (Polymer Laboratories) of porosity 10^5\AA , 10^4\AA , 10^3\AA and 10^2\AA were used, and the molecular weight was determined from a universal polystyrene calibration curve using the Mark-Houwink co-efficients $a = 0.693$, $K = 4.03 \times 10^{-4}$ (high 1,2) and $K = 4.57 \times 10^{-4}$ (high 1,4).

The percentage 1,4 content of the product was determined by ^1H nuclear magnetic resonance (nmr) spectroscopy in which measurements

were carried out on a Varian Associates EM 60MHz spectrometer, samples of the polymer being prepared as 10% w/v solutions in deuteriochloroform.

5 Example 7

The procedure of Example 6 was repeated except the reaction was initiated with tBDP-siloxy lithiohexyl ether from Example 2 rather than with tBDM-siloxy lithiohexyl ether.

10

Example 8

The procedure of Example 6 was repeated except that the reaction was terminated with excess ethylene oxide rather than
15 excess methanol. The usual work up procedure produced a bifunctional polybutadiene, with a hydroxyl group at one end of the chain and a siloxyl group at the other.

Example 9

20

The procedure of Example 6 was repeated except that the reaction was terminated with exactly 0.0055 mol of dichlorodimethylsilane rather than excess methanol. The usual workup procedure
25 produced a difunctional polybutadiene (M_n/M_w between 1.1 and 1.2 and % 1,4 content between 87% and 91%) possessing siloxyl groups at both ends and a central dimethylsilyl chain-linking group.

Example 10

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Siloxyl terminated polybutadiene (1g) from Example 6 was dissolved in tetrahydrofuran (20ml) in a 100ml round bottom 3-necked flask equipped with magnetic follower, serum cap and nitrogen inlet/outlet. Tetra-n-butylammonium fluoride (1.0M) in tetra-
35 hydrofuran (1.1ml) was then added by injection and the reaction

allowed to proceed at 20°C for 2 hours. Afterwards the solution was added dropwise to excess methanol, allowed to settle and the liquors decanted off to yield a pale yellow syrup, which was identified as monofunctional hydroxyl terminated polybutadiene ($M_n/M_w=1.15$, and % 1,4 content=90%).

Example 11

The procedure of Example 10 was repeated using as the starting polymer the siloxy-terminated polybutadiene products of Example 7 rather than the product of Example 6, to yield a monofunctional hydroxy-terminated polybutadiene (M_n/M_w between 1.1 and 1.2, and % 1,4 content between 87% and 91%).

Examples 12 and 13

The procedure of Example 10 was repeated using as the starting polymer the siloxy-terminated polybutadiene products of Examples 8 and 9 in turn rather than the product of Example 6. In both cases, the siloxy groups on the starting polymers were replaced by hydroxy groups, to yield difunctional hydroxy-terminated polybutadienes (M_n/M_w between 1.1 and 1.2, % 1,4 content between 87% and 91%).

Claims

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1. Process for the anionic polymerisation of an olefinic-containing monomer comprising contacting the monomer in an inert solvent with a monofunctional silyl ether initiator of general formula I



wherein R^1, R^2 and R^3 are independently selected from saturated and unsaturated aliphatic and aromatic radicals, A is a hydrocarbon bridging group containing from 1 to 25 carbon atoms, and B is an alkali metal.

2. Process according to claim 1 wherein the solvent is non-polar.
3. Process according to claim 2 wherein the solvent is a hydrocarbon.
4. Process according to claim 3 wherein the solvent is an aliphatic, an alicyclic or an aromatic hydrocarbon having from 3 to 12 carbon atoms.
5. Process according to claim 4 wherein the solvent is an alkane having from 4 to 8 carbon atoms.
6. Process according to any one of the preceding claims wherein the monomer comprises an alkene.
7. Process according to claim 6 wherein the monomer comprises an optionally-substituted styrene or an optionally-substituted vinylnaphthalene.
8. Process according to any one of claims 1 to 5 wherein the monomer comprises a 1,3-diene.

9. Process according to claim 8 wherein the 1,3-diene contains from 4 to 12 carbon atoms per molecule.
10. Process according to claim 9 wherein the 1,3-diene contains from 4 to 8 carbon atoms per molecule.
11. Process according to claim 10 wherein the 1,3-diene comprises isoprene, 2,3-dimethyl-1,3-butadiene, 1,3-pentadiene, or 1,3-butadiene.
12. Process according to claim 11 wherein the 1,3-diene comprises 1,3-butadiene.
13. Process according to any one of the preceding claims wherein R^1 , R^2 and R^3 are independently selected from alkyl, alkoxy, aryl, and alkaryl groups.
14. Process according to claim 13 wherein each of R^1 , R^2 and R^3 contains from 1 to 10 carbon atoms.
15. Process according to claim 14 wherein R^1 , R^2 and R^3 together contain at least 5 carbon atoms.
16. Process according to claim 15 wherein at least one of R^1 , R^2 and R^3 is selected from phenyl and monosubstituted phenyl.
17. Process according to any one of the preceding claims wherein -A- is a saturated hydrocarbon bridging group contain at least 2 carbon atoms.
18. Process according to claim 17 wherein -A- is a branched or straight chain alkyl bridging group.
19. Process according to claim 18 wherein -A- is $-(CH_2)_m-$ where m is an integer from 3 to 15.

20. Process according to any one of the preceding claims wherein B is lithium.
21. Process according to any one of the preceding claims wherein the molar ratio of initiator to monomer is between 0.5 to 1000 and 50 to 1000.
22. Process according to any one of the preceding claims wherein, after propagation has ceased, the living polymer chains are terminated by a proton or a functional group.
23. Process according to claim 22 wherein the functional group comprises a carboxyl, hydroxyl, mercapto, amino or a metal halide group.
24. A process according to any one of claims 1 to 21 wherein, after propagation has ceased, the living polymer chains are linked together by a di- or poly- functional linking agent.
25. Process according to claim 24 wherein the linking agent comprises a halosilane or an organohalide.
26. Process according to any one of claims 22 to 25 wherein, after termination of the living polymer chains, the organosiloxy terminal groups on the polymer chains are desilylated and protonated to convert said groups into functional hydroxyl groups.
27. Siloxy-terminated hydrocarbon polymer containing at least one polymer chain per molecule of general formula II



wherein R^1, R^2 and R^3 are independently selected from saturated and unsaturated aliphatic and aromatic radicals, A is a hydrocarbon bridging group containing from 1 to 25 carbon atoms, and $-(M)_n-$ represents a polymerised olefinic-containing monomer.

28. Polymer according to claim 27 wherein the monomer comprises a 1,3-diene.

29. Polymer according to claim 28 wherein the monomer comprises an optionally substituted styrene or an optionally-substituted vinyl-naphthalene.

30. Polymer according to claim 27 wherein the monomer comprises a 1,3-diene.

31. Polymer according to claim 30 wherein the 1,3-diene contains from 4 to 12 carbon atoms per molecule.

32. Polymer according to claim 31 wherein the 1,3-diene contains from 4 to 8 carbon atoms per molecule.

33. Polymer according to claim 32 wherein the 1,3-diene comprises isoprene, 2,3-dimethyl-1,3-butadiene, 1,3-pentadiene, or 1,3-butadiene.

34. Polymer according to claim 33 wherein the 1,3-diene comprises 1,3-butadiene.

35. Polymer according to any one of claims 27 to 34 wherein R^1, R^2 and R^3 are independently selected from alkyl, alkoxy, aryl, and alkaryl groups.

36. Polymer according to claim 35 wherein each of R^1, R^2 and R^3 contains from 1 to 10 carbon atoms.

37. Polymer according to claim 36 wherein R^1, R^2 and R^3 together contain at least 5 carbon atoms.

38. Polymer according to claim 37 wherein at least one of R^1, R^2 and R^3 is selected from phenyl or monosubstituted phenyl.

39. Polymer according to any one of claims 27 to 38 wherein -A- is a saturated hydrocarbon bridging group contain at least 2 carbon atoms.

40. Polymer according to claim 39 wherein -A- is a branched or straight chain alkyl bridging group.

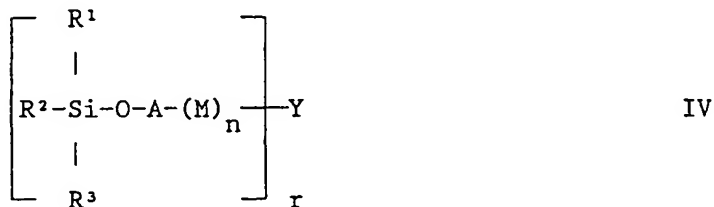
41. Polymer according to claim 40 wherein -A- is $-(CH_2)_m-$ where m is an integer from 3 to 15.

42. Polymer according to any one of claim 27 to 41, of general formula III



where X is selected from H, carboxyl, hydroxy, mercapto, amino, and a metal halide group.

43. Polymer according to any one of claim 27 to 41, of general formula IV



wherein Y is the residue of a multi-functional halide coupling agent containing q functional halide groups, where q is an integer from 2 to 20, and r is an integer of at least 2 which is less or equal to q.

44. Polymer according to any one of claims 27 to 43 wherein $-(M)_n-$ has an average molecular weight of between 1,000 and 100,000.

45. A monofunctional silylether initiator according to any one of the preceding claims 1 and 13 to 19.

46. A method of preparing a monofunctional silyl ether initiator according to claim 45 which comprises reacting, in an inert solvent, an alkali metal B with an organosiloxyhalide of general formula V



where R^1, R^2, R^3 , A and B are as defined in claim 45 and Z^1 is a halogen.

47. A method according to claim 46 wherein Z^1 is chlorine or bromine.

48. A method according to claim 47 wherein B is lithium and Z^1 is chlorine.

49. A method according to any one of claims 46 to 48 wherein the inert solvent is a non-polar solvent.

50. A method according to claim 49 wherein the inert solvent is a hydrocarbon solvent.

51. A method according to any one of claim 46 to 50 wherein the molar ratio of alkali metal to organosiloxyhalide is at least 3:1.

52. A method according to claim 51 wherein the molar ratio of alkali metal to organosiloxyhalide is from 4:1 to 12:1.

53. A process for the anionic polymerisation of an olefinic-containing monomer substantially as hereinbefore described with particular reference to any one of Examples 6 to 9.

54. A siloxy-terminated hydrocarbon polymer substantially as hereinbefore described with particular reference to any one of the Examples 6 to 9.

55. A monofunctional silyl ether initiator substantially as hereinbefore described with particular reference to any one of Examples 1 to 5.

56. A method of preparing a monofunctional silyl ether initiator substantially as hereinbefore described with reference to any one of Examples 1 to 5.

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